

whereby said hydrogen atoms react with said catalyst in said vessel at a pressure less than atmospheric, thereby releasing energy and producing hydrogen atoms having a binding energy of about  $E_b = 13.6/n^2 \text{ eV}$ , where  $n$  is a fraction whose numerator is 1 and denominator is an integer greater than 1.

53. A cell according to claim 52, wherein said gaseous catalyst comprises hydrogen atoms having a binding energy of about  $E_b = 13.6/n^2 \text{ eV}$ , where  $n$  is a fraction whose numerator is 1 and denominator is an integer greater than 1.

54. A cell according to claim 52, wherein said cell maintains the reaction,

$$m \times 27.21 \text{ eV} + H \left[ \frac{a_H}{m'} \right] + H \left[ \frac{a_H}{p} \right] - H^+ + e^- + H \left[ \frac{a_H}{(p+m)} \right] + [(p+m)^2 - p^2 - (m'^2 - 2m)] \times 13.6 \text{ eV}$$

$$H^+ + e^- \rightarrow H \left[ \frac{a_H}{1} \right] + 13.6 \text{ eV}$$

$$H \left[ \frac{a_H}{m'} \right] + H \left[ \frac{a_H}{p} \right] - H \left[ \frac{a_H}{1} \right] + H \left[ \frac{a_H}{(p+m)} \right] + [2pm + m^2 - m'^2] \times 13.6 \text{ eV} + 13.6 \text{ eV}$$

where  $m$  and  $p$  are positive non-zero integers,  $m'$  is an integer greater than 1, and  $a_H$  is the radius of the hydrogen atom ( $n=1$ ).

55. A cell according to claim 52, whereby said gaseous hydrogen atoms are formed in the cell by reacting molecules containing hydrogen atoms, and

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a second catalyst for disassociating said molecules to produce hydrogen atoms.

56. A cell according to claim 55, wherein said second catalyst is at least one element selected from the group consisting of transition elements and lanthanides.

57. 6 A cell according to claim 55, 4 wherein said second catalyst is at least one element selected from the group consisting of the refractory metals, activated charcoal, platinum, palladium, gold, rhenium and iridium.

58. 7 A cell according to claim 55, 4 further comprising a valve for controlling the flow of said molecules over said second catalyst.

59. A cell according to claim 52, wherein said gaseous catalyst is adapted to sublime, boil, or volatilize when heated.

60. 9 A cell according to claim 52, 1 wherein said gaseous catalyst is formed from a salt.

61. 10 A cell according to claim 60, 9 wherein said salt is selected from the group consisting of halides, sulfates, phosphates, carbonates, hydroxides, and sulfides.

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A cell according to claim 60, wherein said gaseous catalyst is formed from a salt of rubidium or potassium.

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A cell according to claim 62, wherein said salt of potassium is selected from the group consisting of KF, KCl, KBr, KI,  $K_2S_2$ , KOH,  $K_2SO_4$ ,  $K_2CO_3$ ,  $K_2PO_4$ , and  $K_2GeF_4$ .

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64.

A cell according to claim 62, wherein said salt of rubidium is selected from the group consisting of RbF, RbCl, RbBr, RbI,  $Rb_2S_2$ , RbOH,  $Rb_2SO_4$ ,  $Rb_2CO_3$ , and  $Rb_3PO_4$ .

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65.

A cell according to claim 52, wherein said gaseous catalyst comprises a cation having a vapor pressure greater than zero when said gaseous catalyst is heated, said cation being selected from the group consisting of ( $K^+$ ), ( $Rb^+$ ), ( $Mo^{2+}$ ), and ( $Ti^{2+}$ ).

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66.

A cell according to claim 52, wherein said gaseous catalyst comprises a pair of cations having a vapor pressure greater than zero when said gaseous catalyst is heated, said pair of cations being selected from the group consisting of: ( $Sn^{4+}$ ,  $Si^{4+}$ ), ( $Pr^{3+}$ ,  $Ca^{2+}$ ), ( $Sr^{2+}$ ,  $Cr^{2+}$ ), ( $Cr^{3+}$ ,  $Tb^{3+}$ ), ( $Sb^{3+}$ ,  $Co^{2+}$ ), ( $Bi^{3+}$ ,  $Ni^{2+}$ ), ( $Pd^{2+}$ ,  $In^+$ ), ( $La^{3+}$ ,  $Dy^{3+}$ ), ( $La^{3+}$ ,  $Ho^{3+}$ ), ( $K^+$ ,  $K^+$ ), ( $V^{3+}$ ,  $Pd^{2+}$ ), ( $Lu^{3+}$ ,  $Zn^{2+}$ ), ( $As^{3+}$ ,  $Ho^{3+}$ ), ( $Mo^{5+}$ ,  $Sn^{4+}$ ), ( $Sb^{3+}$ ,  $Cd^{2+}$ ), ( $Ag^{2+}$ ,  $Ag^+$ ), ( $La^{3+}$ ,  $Er^{3+}$ ), ( $V^{4+}$ ,  $B^{3+}$ ), ( $Fe^{3+}$ ,  $Ti^{3+}$ ), ( $Co^{2+}$ ,  $Ti^+$ ), ( $Bi^{3+}$ ,  $Zn^{2+}$ ), ( $As^{3+}$ ,  $Dy^{3+}$ ), ( $Ho^{3+}$ ,  $Mg^{2+}$ ), ( $K^+$ ,  $Rb^+$ ), ( $Cr^{3+}$ ,  $Pr^{3+}$ ), ( $Sr^{2+}$ ,  $Fe^{2+}$ ), ( $Ni^{2+}$ ,  $Cu^+$ ), ( $Sr^{2+}$ ,  $Mo^{2+}$ ),

(Y<sup>3+</sup>, Zr<sup>4+</sup>), (Cd<sup>2+</sup>, Ba<sup>2+</sup>), (Ho<sup>3+</sup>, Pb<sup>2+</sup>), (Pd<sup>2+</sup>, Li<sup>+</sup>), (Eu<sup>3+</sup>, Mg<sup>2+</sup>), (Er<sup>3+</sup>, Mg<sup>2+</sup>), (Bi<sup>4+</sup>, Al<sup>3+</sup>), (Ca<sup>2+</sup>, Sm<sup>3+</sup>), (V<sup>3+</sup>, La<sup>3+</sup>), (Gd<sup>3+</sup>, Cr<sup>2+</sup>), (Mn<sup>2+</sup>, Tl<sup>+</sup>), (Yb<sup>3+</sup>, Fe<sup>2+</sup>), (Ni<sup>2+</sup>, Ag<sup>+</sup>), (Zn<sup>2+</sup>, Yb<sup>2+</sup>), (Se<sup>4+</sup>, Sn<sup>4+</sup>), (Sb<sup>3+</sup>, Bi<sup>2+</sup>), and (Eu<sup>3+</sup>, Pb<sup>2+</sup>).

<sup>16</sup>  
~~67.~~ A cell according to claim 52, wherein said gaseous catalyst comprises an ionic compound resistant to reduction by hydrogen atoms.

<sup>17</sup>  
~~68.~~ A cell according to claim 52, wherein said gaseous catalyst is adapted to provide ions.

<sup>18</sup>  
~~69.~~ A cell according to claim 52, whereby said vessel maintains a hydrogen partial pressure of less than about one torr.

~~70.~~ A cell according to claim 52, wherein said vessel maintains said catalyst in molten form.

~~71.~~ A cell according to claim 52, wherein the temperature of said vessel is maintained at about 50 °C above the melting point of said gaseous catalyst.

~~72.~~ A cell according to claim 52, wherein the hydrogen partial pressure in said vessel is maintained at about 200 millitorr.

~~73.~~ A cell according to claim 66, wherein the temperature of said vessel is maintained at about 50 °C above the higher melting point of compounds of the two cations comprising said cation pair of said gaseous catalyst.

~~74.~~<sup>23</sup> A cell according to claim ~~52~~, further comprising a valve for selectively releasing said catalyst from said vessel.

~~75.~~<sup>24</sup> A cell according to claim ~~52~~, further comprising a valve for selectively releasing said hydrogen atoms having a binding energy of about  $E_b = 13.6/n^2$  eV, where  $n$  is a fraction whose numerator is 1 and denominator is an integer greater than 1.

~~76.~~ A cell according to claim 52, wherein the vapor partial pressure of said gaseous catalyst varies with temperature.

~~77.~~<sup>26</sup> A cell according to claim ~~52~~, further comprising a heater for heating said vessel.

~~78.~~ A cell according to claim 52, further comprising a catalyst reservoir communicating with said reaction vessel, said catalyst reservoir containing said gaseous catalyst or a source thereof.

<sup>28</sup>  
~~79~~. A cell according to claim <sup>27</sup>~~78~~, further comprising a heater for heating said catalyst.

<sup>29</sup>  
~~80~~. A cell according to claim <sup>27</sup>~~78~~, wherein said catalyst reservoir is external to said reaction vessel.

<sup>30</sup>  
~~81~~. A cell according to claim <sup>29</sup>~~80~~, further comprising a flow control valve for controlling the flow of said catalyst from said catalyst reservoir into said vessel.

<sup>31</sup>  
~~82~~. A cell according to claim <sup>1</sup>~~52~~, further comprising a chamber for containing hydrogen atoms or a source of hydrogen atoms communicating with said reaction vessel.

<sup>32</sup>  
~~83~~. A cell according to claim <sup>31</sup>~~82~~, further comprising a flow control valve for controlling the flow of hydrogen atoms from said chamber into said vessel.

<sup>33</sup>  
~~84~~. A cell according to claim <sup>82 31</sup>~~832~~ wherein said source of hydrogen atoms comprises an internal combustion engine.

<sup>85</sup>. A cell according to claim 82, wherein said source of hydrogen atoms comprises a tungsten capillary heated to between 1800 and 2000 K for dissociating molecules containing hydrogen atoms to produce hydrogen atoms.

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A cell according to claim ~~85~~, further comprising a valve for controlling the flow of said molecules over said tungsten capillary.

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A cell according to claim ~~82~~, wherein said source of hydrogen atoms comprises an inductively coupled plasma flow tube for dissociating molecules containing hydrogen atoms to produce hydrogen atoms.

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A cell according to claim ~~87~~, further comprising a valve for controlling the flow of said molecules into said inductively coupled plasma flow tube.

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A cell according to claim ~~87~~, further comprising a power controller for controlling the power dissipated in said inductively coupled plasma flow tube.

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A cell according to claim ~~52~~, further comprising a heat exchanger for removing said extracted energy from said cell.

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A cell according to claim ~~52~~, further comprising a power gauge for measuring the amount of extracted <sup>power</sup> ~~energy~~ in said cell.

92. A method for extracting energy from hydrogen comprising the steps

of:

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providing a gaseous catalyst having a net enthalpy of reaction of about  $27 * (p/2) \text{ eV}$ , where  $p$  is an integer greater than 1;  
providing gaseous hydrogen atoms; and  
reacting said gaseous catalyst with said gaseous hydrogen atoms, thereby producing hydrogen atoms having a binding energy of about  $E_b = 13.6/n^2 \text{ eV}$ , where  $n$  is a fraction whose numerator is 1 and denominator is an integer greater than 1,  
said reaction occurring at a pressure less than atmospheric pressure.

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93. A method according to claim 92, wherein said gaseous hydrogen atoms are provided by disassociating molecules containing hydrogen atoms.

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94. A method according to claim 92, wherein gaseous hydrogen atoms are provided by contacting molecules containing hydrogen atoms with a <sup>second catalyst</sup> catalyst for disassociating said molecules to produce hydrogen atoms in the gas phase.

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95. A method according to claim 92, wherein said gaseous catalyst comprises gaseous hydrogen atoms having a binding energy of about  $E_b = 13.6/n^2 \text{ eV}$ , where  $n$  is a fraction whose numerator is 1 and denominator is an integer greater than 1.

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96. A method according to claim 92, wherein said gaseous catalyst is provided according to the reaction,



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$$m \times 27.21 \text{ eV} + H \left[ \frac{a_H}{m'} \right] + H \left[ \frac{a_H}{p} \right] - H^+ + e^- + H \left[ \frac{a_H}{(p+m)} \right] + [(p+m)^2 - p^2 - (m'^2 - 2m)] \times 13.6 \text{ eV}$$

$$H^+ + e^- - H \left[ \frac{a_H}{1} \right] + 13.6 \text{ eV}$$

$$H \left[ \frac{a_H}{m'} \right] + H \left[ \frac{a_H}{p} \right] - H \left[ \frac{a_H}{1} \right] + H \left[ \frac{a_H}{(p+m)} \right] + [2pm + m^2 - m'^2] \times 13.6 \text{ eV} + 13.6 \text{ eV}$$

where m and p are positive non-zero integers, m' is an integer greater than 1, and a<sub>H</sub> is the radius of the hydrogen atom (n=1).

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A method according to claim 92, wherein said gaseous catalyst is provided by volatilizing a material to a gaseous state and ionizing said gaseous material.

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A method according to claim 92, wherein said hydrogen atoms are provided by flowing gaseous molecules containing hydrogen atoms over a hot refractory metal, transition metal, platinum, palladium, gold, rhenium, or iridium.

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A method according to claim 92, wherein said hydrogen atoms are provided by flowing gaseous molecules containing hydrogen atoms over a tungsten capillary heated by electron bombardment to between 1800 and 2000 K.

<sup>153</sup>  
100. A method according to claim <sup>145</sup>92, wherein said hydrogen atoms are provided by flowing gaseous molecules containing hydrogen atoms in an inductively coupled plasma flow tube.

<sup>154</sup>  
101. A method according to claim <sup>145</sup>92, wherein said reaction occurs at a pressure less than about one torr.

<sup>155</sup>  
102. A method according to claim <sup>145</sup>92, wherein the partial pressure of hydrogen atoms in the reaction is less than about one torr.

<sup>156</sup>  
103. A method according to claim <sup>145</sup>92, wherein the partial pressure of hydrogen atoms in the reaction is about 200 millitorr.

104. A method according to claim 92, wherein the partial pressure of the gaseous catalyst in the reaction is between about 50 and 250 millitorr.

<sup>157</sup>  
105. A method according to claim <sup>145</sup>92, wherein said reaction occurs at a temperature of about 50 °C above the melting point of said gaseous catalyst.

<sup>158</sup>  
106. A method according to claim <sup>145</sup>92, wherein the vapor partial pressure of said gaseous catalyst is controlled by varying the temperature of said gaseous catalyst.